



Gaswärme-Institut e.V.
Essen

State-of-the-art oxyfuel solutions for
reheating and annealing furnaces in
steel industry

Dr.-Ing. Axel Scherello

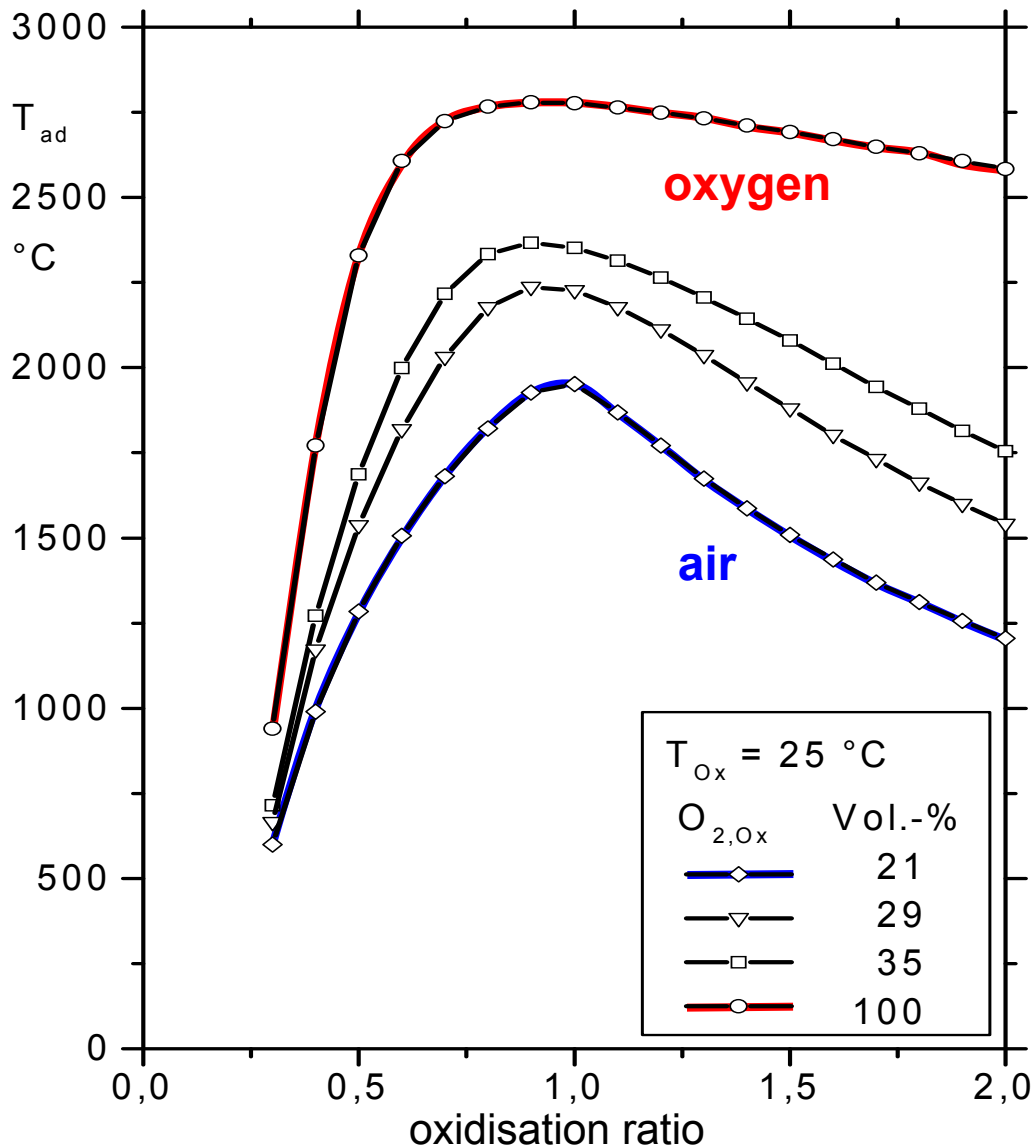
- Axel Scherello, Gaswärme-Institut e. V. Essen, Germany
- Werner Högner, ThyssenKrupp Steel AG, Duisburg, Germany
- Erik Claesson, Ovako Steel AB, Hofors, Sweden
- Pete Bamforth, Outokumpu Stainless AB, Nyby, Sweden
- Christophe Mercier, Ascométal SA, Fos-sur-Mer, France

- Introduction
 - temperatures
 - energy
 - scale formation
- Examples
 - Soaking pit furnaces
 - Rotary hearth furnaces
 - Stainless steel strip annealing
 - Carbon steel strip galvanising
- Conclusion

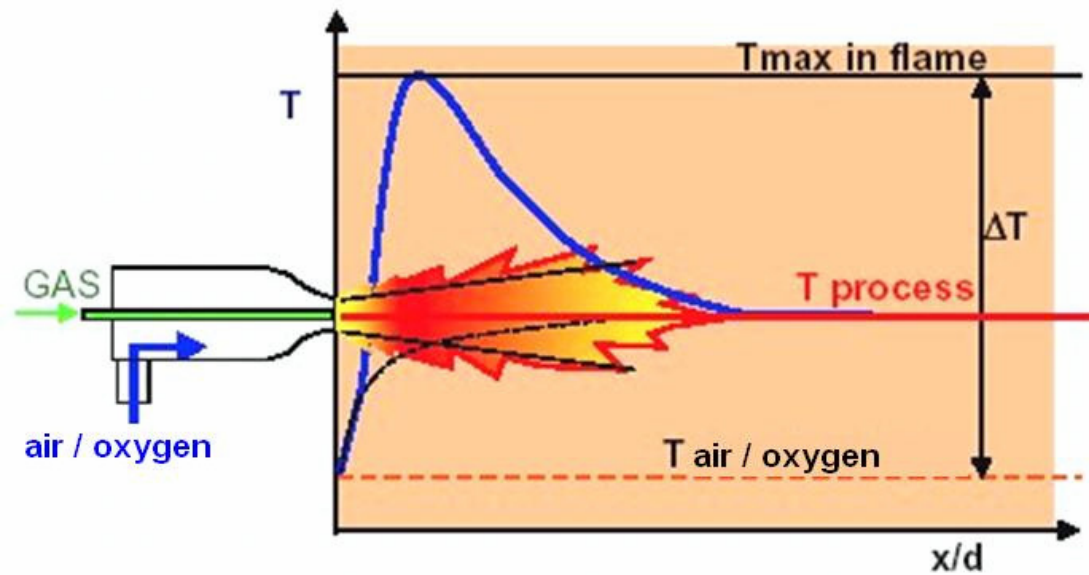
- no nitrogen ballast
- high efficiency – no heat recovery equipment
- moderate peak temperatures even using oxygen
- reduced scale formation
- steel production is a combination of process steps – demand for flexibility
- increased throughput capacity and higher flexibility using oxyfuel

- costs for O₂

explanations & examples



theoretical adiabatic combustion temperature using high calorific natural gas and different oxidators

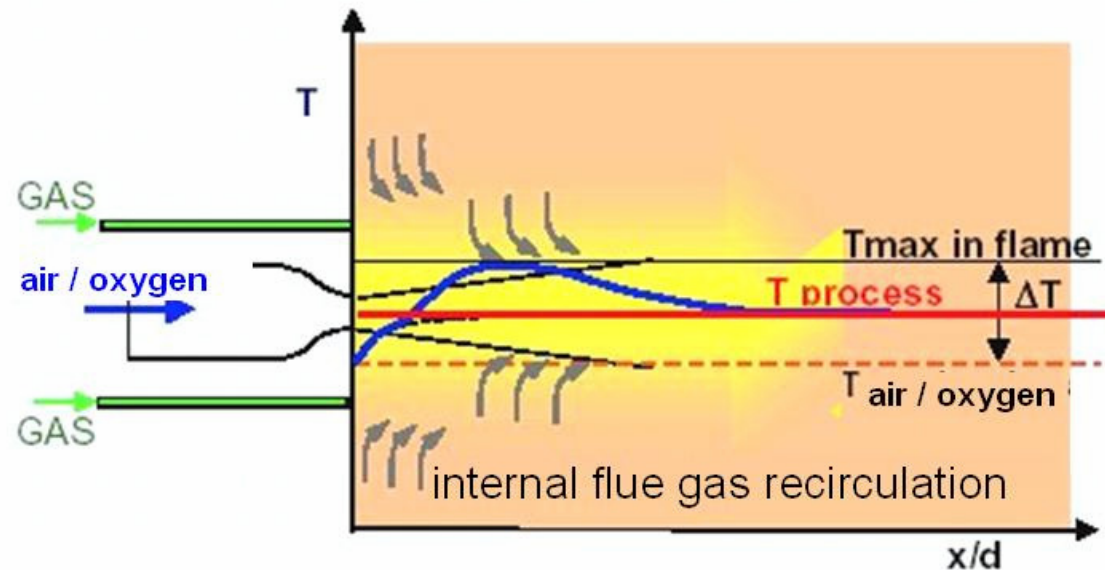


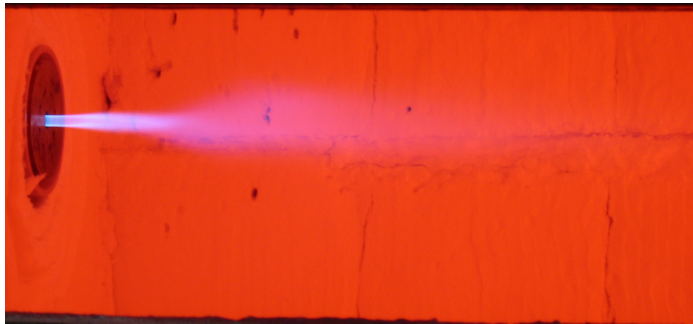
standard combustion

moderate temperatures
based on internal flue gas
recirculation

state of the art

- diluted combustion
- mild combustion
- flameless oxidation
- flameless oxyfuel





oxyfuel staged combustion
with 5 % primary oxygen

0 350 700 mm



flameless oxyfuel

0 500 1000 mm

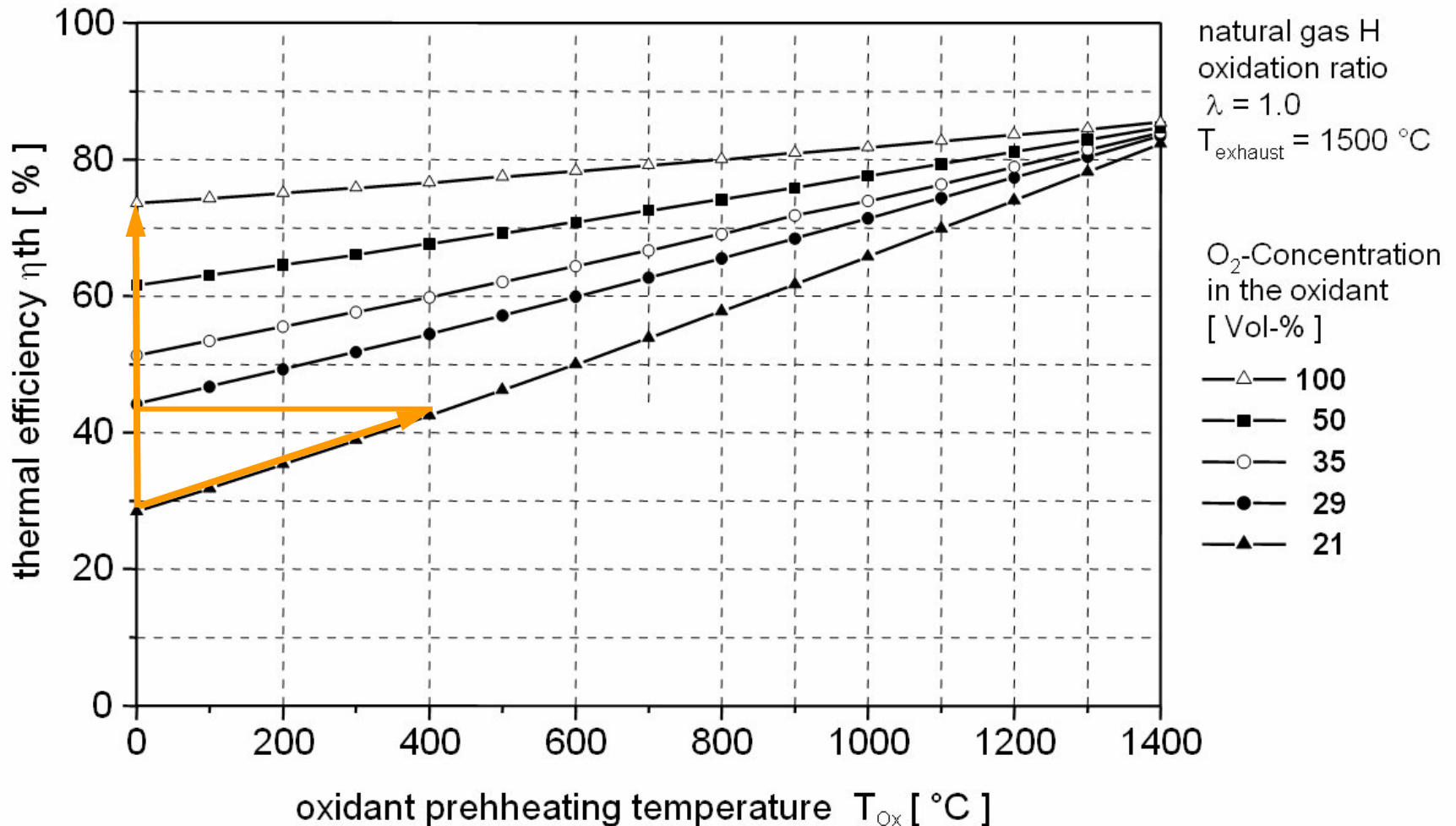
$$\dot{m}_{scale} = f(p_{O_2}, \Delta t, \dots)$$

- recirculation and dilution due to flue gas entrainment
- reduced local partial pressures of O₂
- avoiding temperature peaks
- reduced resident time of product in furnace



reduced scale formation

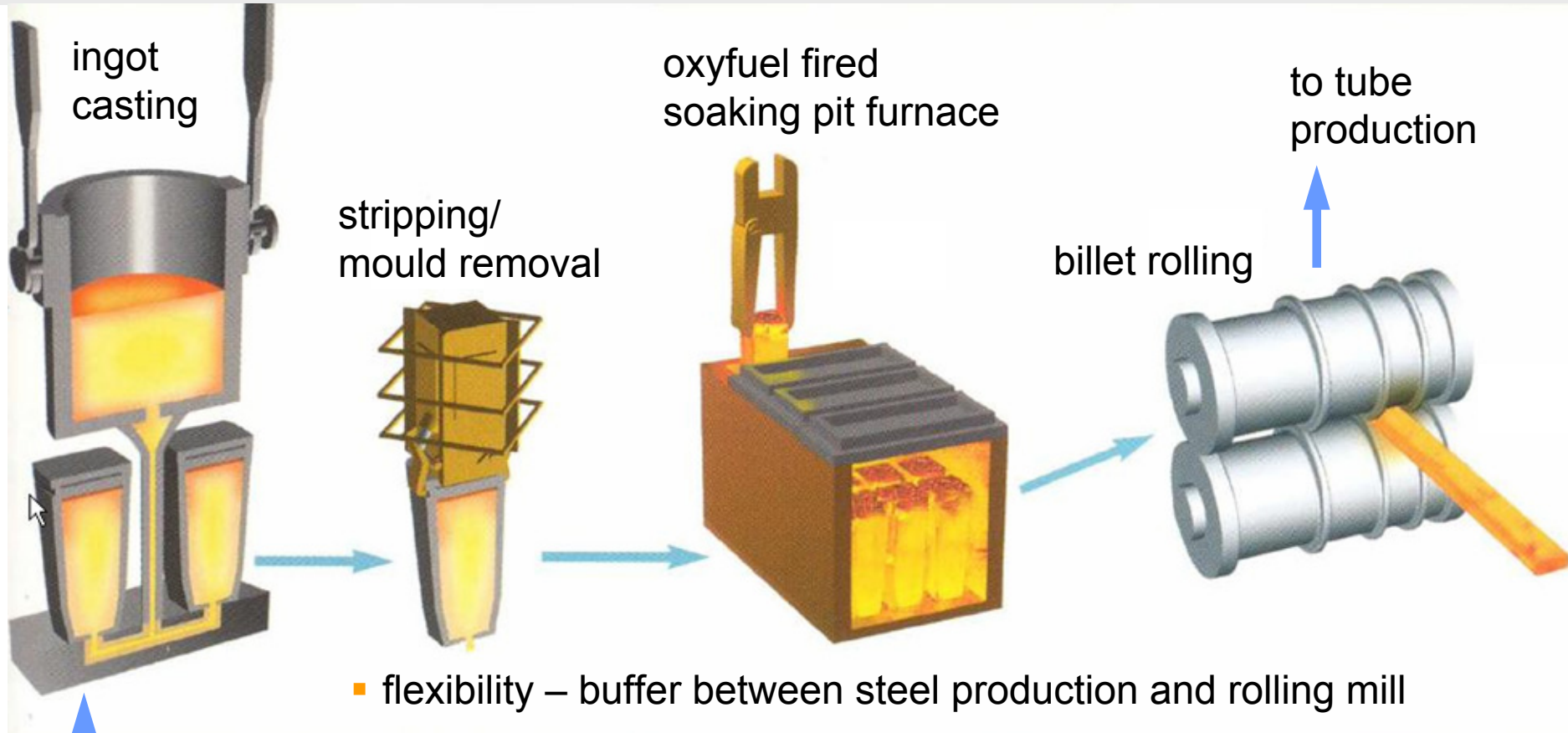
high efficiency for oxyfuel – even without heat recovery



Ovako – soaking pit furnaces



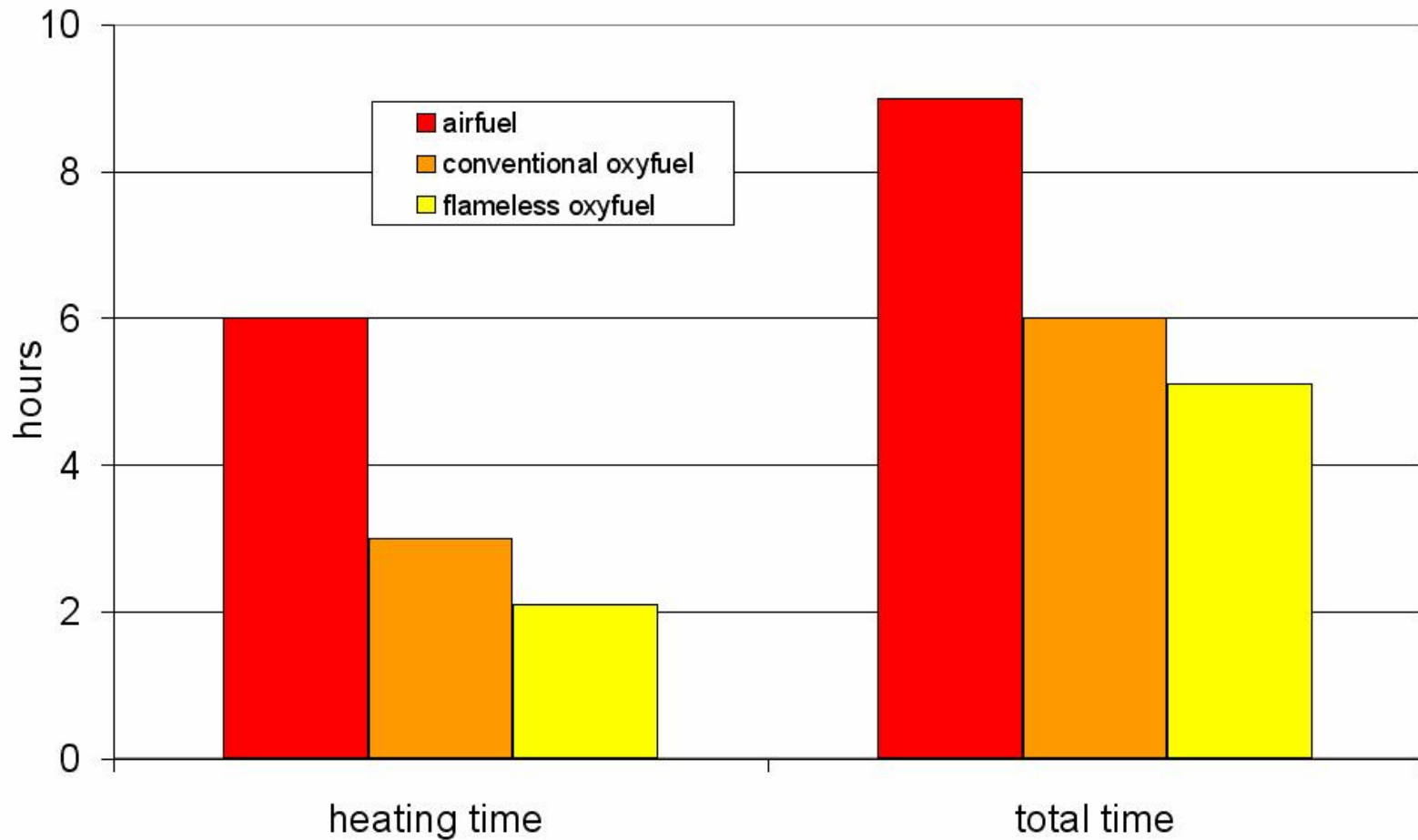
48 furnaces converted to oxyfuel combustion at Ovako Steel, Horfors works, Sweden



from electric arc melting

- flexibility – buffer between steel production and rolling mill
 - low energy consumption
 - increased throughput (> 30 %)
- decreased scale formation rate – especially for flameless oxyfuel

6 → 2 reduction of heating time 9 → 5 reduction of total time





advantages

- compact exhaust gas system
- reduced constructive amount
- decreased and simplified maintenance
- lower investment costs
- no recuperators and electrical ventilators
- 30-45 % ↓ specific fuel consumption
- pollutant emissions reduction *

airfuel

- 1 m³/h natural gas, 35 MJ/m³
- 9.5 m³ air (2 m³ O₂, 7.5 m³ N₂)
- hypothetical NO_x formation
2000 mg/h absolute
- flue gas 10.5 m³/h
 - 1 CO₂, 2 H₂O, 7.5 N₂
- dry flue gas 8.5 m³/h
- 235 mg/m³ NO_x



not comparable!

oxyfuel

- 1 m³/h natural gas, 35 MJ/m³
- 2 m³ oxygen
- hypothetical NO_x formation
2000 mg/h absolute
- flue gas 3 m³/h
 - 1 CO₂, 2 H₂O
- dry flue gas 1 m³/h
- 2000 mg/m³ NO_x

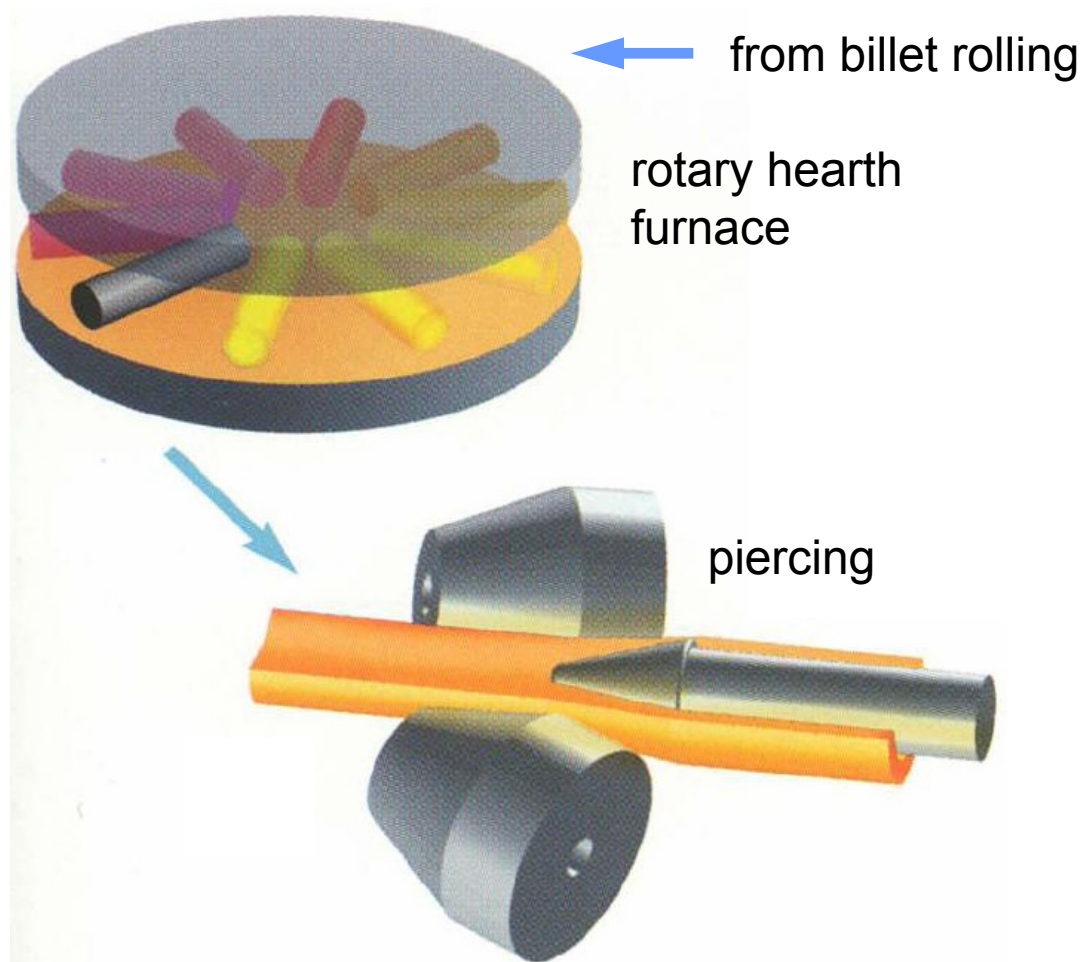
2000 mg/h : 35 MJ/h =

- 57 mg/MJ NO_x

2000 mg/h : 35 MJ/h =

- 57 mg/MJ NO_x

- soaking pit furnaces used to reheat ingots prior to rolling
- first flameless oxyfuel installation in 2004 – replacing airfuel equipment like burners, air ducts, recuperators and blowers
- targets
 - 33 % shorter heating cycles
 - 40 % reduced specific fuel consumption
 - 40 % decreased NO_x emissions
- improved heating characteristics
- less scale formation
- only 9 instead of 13 furnaces deliver same production rate
- energy cost savings, reduced maintenance and improved logistics



- 290 kWh/t for cold charged material
- 1120 to 1270 °C final product temperature



- simple and compact oxyfuel installations at Ovako rotary hearth furnace

Compared with airfuel operation

- higher throughputs > 30 %
- lower emission levels < 100 mg/MJ with staged oxyfuel
- decreased energy consumption
- more uniform heating < 10 °C from top to bottom

Until now oxyfuel burners with staged combustion

- flameless oxyfuel combustion for
 - further more uniform heating
 - higher throughputs
 - lower NO_x emissions

Nyby works, SE, catenary furnace on the preparatory annealing line

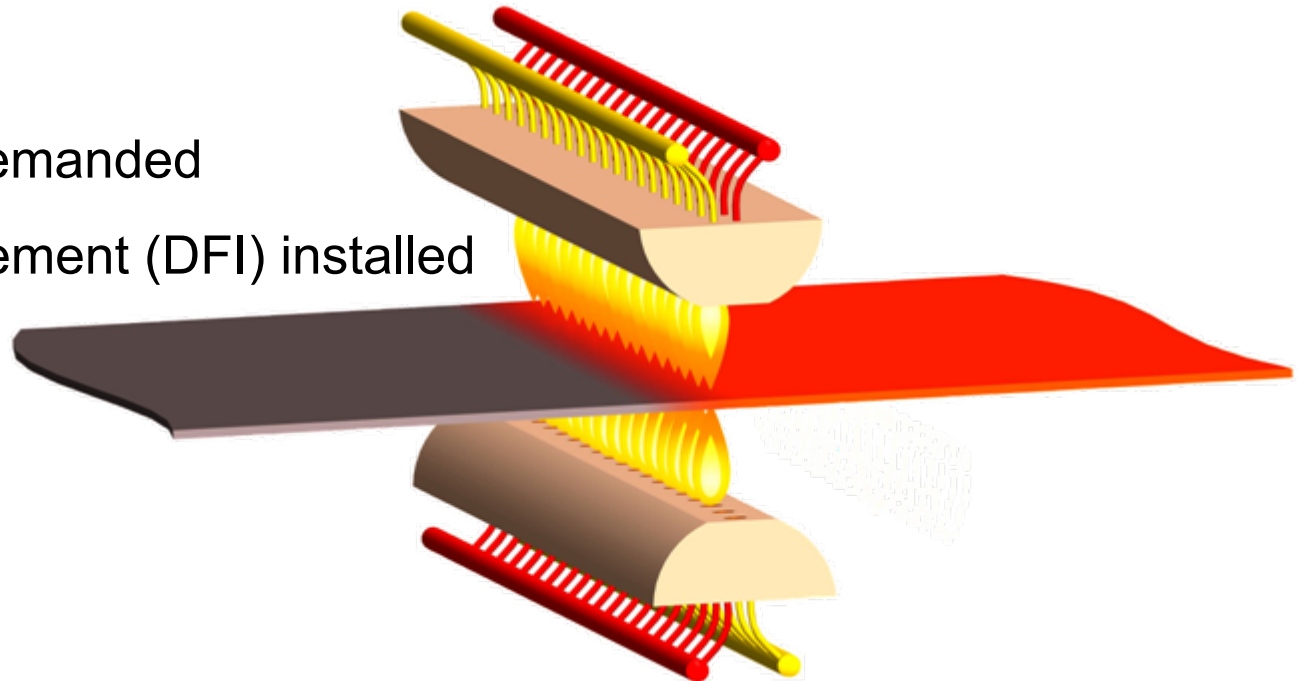
- equipped with flameless oxyfuel burners
 - high stirring rates of furnace atmospheres
 - increased heat transfer rates towards the product
 - small level of NO_x formation
 - flexibility
-
- throughput growth of about 55 %
 - same pickling amount – decreased scale formation
 - NO_x emissions were kept below 70 mg/MJ
 - specific fuel consumption reduction 40 %

second catenary furnace at finish annealing line

- change from airfuel to oxyfuel
- production capacity increase from 11 to 23 tons per hour

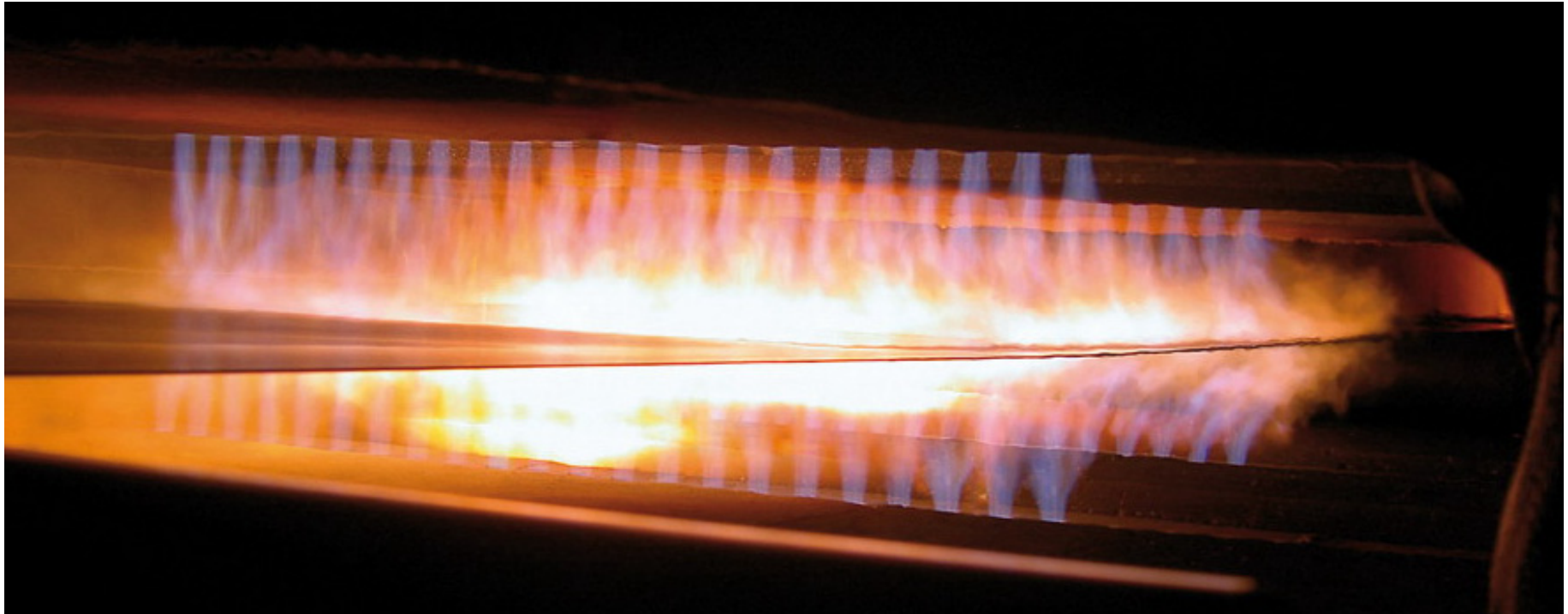
additional capacity demanded

- direct flame impingement (DFI) installed

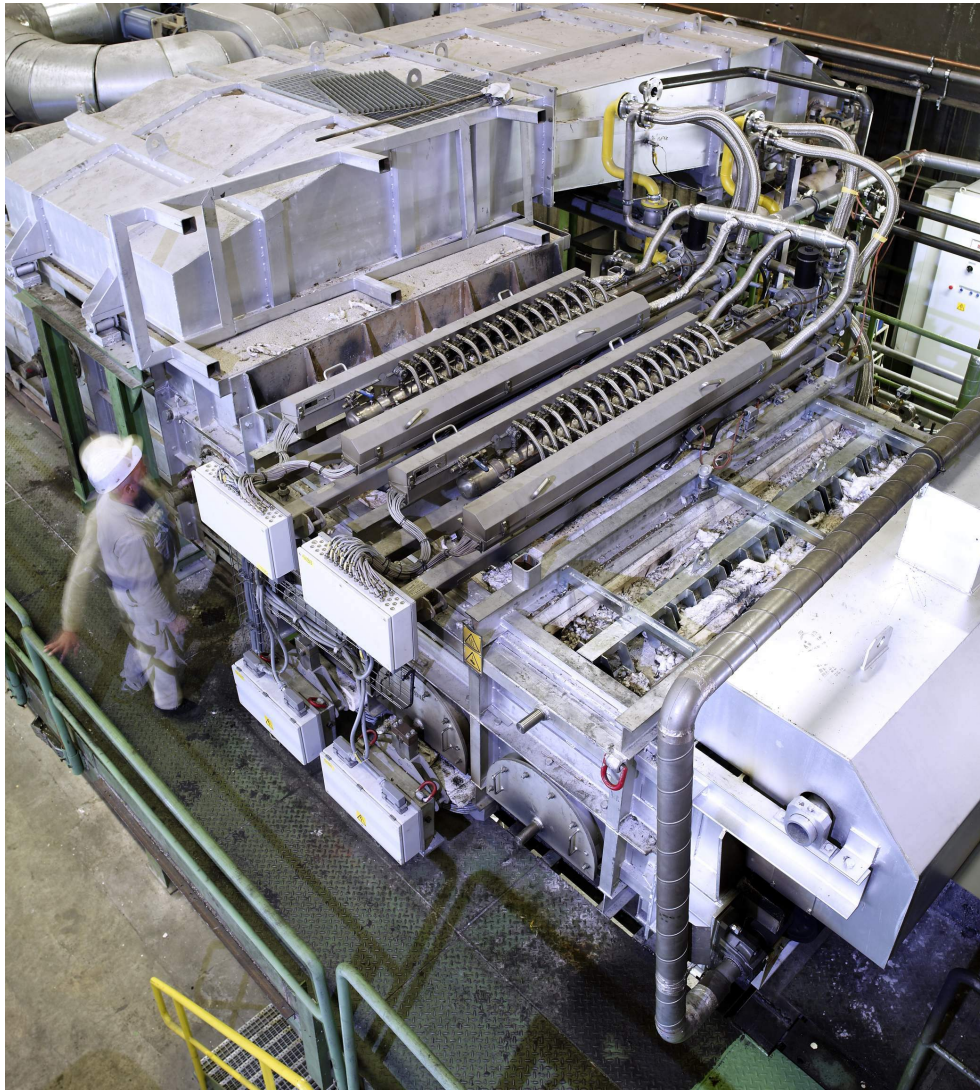


- DFI unit: 120 burner nozzles, 4 burner rows
- heat input 4 MW
- length 1.8 m
- 50 % additional capacity increase
even for highly reflecting stainless steel strip
- improved temperature control
- flexibility





- DFI oxyfuel unit 5 MW
- additional heat input: ΔT 200 °C at 105 t/h
- 30 % throughput increase
- compact design 3 m
- unit fits into existing line
- instead of recuperative zone



- precise tuning of strip characteristics
 - surface properties
 - inner temperature distribution
- 25 m pre-cleaning section not necessary any more
- advantages
 - capacity and quality
 - energy savings
 - no pre-cleaning costs
- oxygen supply costs small compared with advantages

- advantages told by plant operators:
 - energy savings
 - increased capacity
 - lower pollutant emissions
 - less but correct scale formation
 - uniform product temperature distribution
 - improved product quality

- oxyfuel combustion with high thermal efficiency
- easy to set up heating systems – reduced maintenance
- oxyfuel application advantageous independent from the used fuel – also for low-calorific fuels
- using combustion knowledge and production experience oxyfuel can be applied with additional economical benefits



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